

CLAIMS

1. Process for heat treatment of a hydrocarbon feedstock in a furnace that comprises at least one radiation chamber with radiant walls, comprising at least one essentially vertical exchange tube bundle inside of which circulates the hydrocarbon feedstock to be treated, whereby said radiant walls are equipped with catalytic radiant burners with porous panels that are typically used in the form of essentially horizontal or optionally vertical bands, distributed over several levels in the vertical direction, or respectively in the horizontal direction, whereby these catalytic burners generate a mean temperature  $T_m$  of the radiant walls of between  $900^{\circ}\text{C}$  and  $1300^{\circ}\text{C}$ , characterized in that ratio  $R$  of the cumulative surface of the porous panels to the cumulative surface of the radiant walls is at least equal to 0.3 and in that this ratio  $R$  is high enough and mean temperature  $T_m$  is low enough so that the  $\text{NO}_x$  level in the smoke at the outlet of the furnace is at most equal to  $100 \text{ mg/NM}^3$ .
2. Process according to claim 1, wherein ratio  $R$  of the cumulative surface area of the porous panels to the cumulative surface area of the radiant walls is at least equal to 0.3 and wherein this ratio  $R$  is high enough, and mean temperature  $T_m$  is low enough, for the  $\text{NO}_x$  level in the smoke at the furnace outlet to be at most equal to  $10 \text{ mg/NM}^3$ .

3. Process according to one of claims 1 and 2, wherein  $T_m$  is between 950°C and 1250°C, and R is between 0.5 and 1.
4. Process according to one of claims 1 to 3, wherein each radiant burner consists of a parallelepipedic box that has one of its faces placed against one of the lateral walls of the furnace, whereby the face opposite to the preceding one consists of a porous panel whose inside face communicates with a fuel supply chamber, and the outside radiative face transfers its heat to the tube bundle essentially by radiation.
5. Process according to one of claims 1 to 4, wherein the porous panel exhibits a pore size of between 0.1 and 0.95, and preferably between 0.3 and 0.8.
6. Process according to any of claims 1 to 5, wherein the combustion of the air-fuel mixture that is used in the supply of catalytic radiant burners takes place in a catalytic zone that is located inside the porous panel, according to a so-called "radiant" combustion mode.
7. Process according to any of claims 1 to 6, wherein the combustion of the air-fuel mixture that is used in the supply of catalytic radiant burners takes place over the outside surface of the porous panel according to a so-called "blue flame" method.
8. Process according to any of claims 1 to 7, wherein at each catalytic radiant burner, the so-called "radiant" combustion mode is used in a

heat flow range that goes from 10 to 600 kW/m<sup>2</sup> and preferably from 100 to 300 kW/m<sup>2</sup>.

9. Process according to any of claims 1 to 8 for steam-cracking hydrocarbons for the production of ethylene and propylene.
10. Process according to any of claims 1 to 8 for vaporeforming of hydrocarbons that have essentially less than 12 carbon atoms for the production of synthesis gas.